This listing of claims will replace all prior versions, and listings, of claims in the subject application:

- 1. (currently amended) A process for regenerating a hydrocarbon conversion catalyst comprising zeolite L, the process comprising contacting the catalyst with ozone at regeneration conditions and absent a halogen-containing compound oxidizable by ozone at the regeneration conditions, the contacting occurring at a temperature of from about 20 to a pout 250°C.
- 2. (original) The process of Claim 1 further characterized in that the catalyst has coke deposited thereon, and the process comprises removing at least a portion of the coke from the catalyst.
 - 3. (canceled)
- 4. (original) The process of claim 1 further characterized in that the contacting occurs at a partial pressure of ozone of up to about 101.3 kPa(g).
- 5. (previously presented) The process of claim 1 further characterized in that the contacting of the catalyst with ozone comprises contacting the catalyst with an ozone-containing gas having a concentration of ozone of from about 0.1 to about 5 mol-%.
- 6. (original) The process of claim 1 further characterized in that the zeolite L contains a metal selected from the group consisting of metals in IUPAC Group 6 (VI A), IUPAC Group 7 (VII A), IUPAC Group 8-10 (VIII A), and IUPAC Group 14 (IV B) of the Periodic Table of the Elements.
- 7. (previously presented) A process for at least partially reactivating a coked zeolite L-containing reforming catalyst, the process comprising contacting the catalyst with a gaseous stream comprising ozone and at least one of air and oxygen and containing from about 0.1 to about 5.0 mol-% ozone, at conditions comprising a temperature of from about 20 to about 250°C and a gas hourly space velocity of up to about 10,000 hr⁻¹, and absent a halogen-containing compound oxidizable by ozone at the regeneration conditions, the conditions being sufficient to burn at least a portion of the coke on the catalyst.

8-21. (canceled)